AD-A242 900



THERMALLY REGENERATIVE FUEL CELLS CONTRACT N00014-89-C-0071



FINAL REPORT OCTOBER 1991

PREPARED FOR:

OFFICE OF NAVAL RESEARCH DEPARTMENT OF THE NAVY 800 NO. QUINCY STREET ARLINGTON, VA 22217-5000

This document has been approved for public release and sale; its distribution is unlimited.

F.A. LUDWIG

PRINCIPAL INVESTIGATOR

J. MCHARDY A. KINDLER CO-PRINCIPAL INVESTIGATORS

D. I. BASIULIS, MANAGER
MATERIALS SCIENCE DEPARTMENT

91 1125 119

91-16508

OFFICE OF NAVAL RESEARCH FINAL REPORT

on

CONTRACT:N00014-89-C-0071

R&T Code 5000 Ser 1113/91/RAD

THERMALLY REGENERATIVE FUEL CELLS

Program Manager D. I. Basiulis Principal Investigator F. A. Ludwig Co-principal Investigators A. Kindler; J. McHardy

NTIS CTIC Union	CRAAS JOHNSON SIGNAS	
By Distrit	oution /	
	Availability is a	;
Dist	Aveil to a constant	:
A-1		ì

HUGHES AIRCRAFT COMPANY ELECTRO-OPTICAL AND DATA SYSTEMS GROUP TECHNOLOGY SUPPORT DIVISION 2000 EAST EL SEGUNDO BOULEVARD PO BOX 902, EL SEGUNDO, CA 90245

Submitted OCTOBER 1991

Reproduction in whole or in part is permitted for any purpose of the United States Government. This document has been approved for public release and sale: its distribution is unlimited.

Program Manager: Danute I. Basiulis
Principal Investigator: Frank A. Ludwig
Telephone Number: (213) 616-6035

Co-principal Investigators: John McHardy; Andrew Kindler

Cognizant ONR Scientific Officers: James Auborn; Robert Nowak

Description of Project:

The three-phase project was undertaken to investigate solventless ionic liquids as pc fluids for a new type of thermally regenerative fuel cell (TRFC). The heart of the invented at Hughes Aircraft Company in 1983¹, is an electrochemical concentration c and base streams react to produce electrical energy. Thermal energy is then used to c resulting salts and regenerate the cell reactants. In principle, a TRFC can be matched of thermal energy simply by selecting working fluids with the appropriate regeneration However, aqueous working fluids (the focus of previous studies) impose limitations operating temperatures and the achievable energy densities. It was the need to overlimitations that prompted the present investigation. Specific aims were to identify post fluids for TRFC systems with both low (200°C) and high (≥700°C) regeneration tempera

Phase I

A major advantage of our aqueous-fluid TRFC systems has been the ability to unelectrodes. The low activation and mass transfer losses of these electrodes contribute to overall system efficiency. Professor Robert A. Osteryoung pointed out that this advance be extended to molten salt (ionic liquid) systems by using mixed Lewis and Brönste acids. Based on his own work with low-melting point molten salts, he suggested that we the fluid system HCl/1-methyl,3-ethylimidazolium chloride (HCl/MEICl). In this system, the reactions are:

The second of old blue the second and the second of old blue the second of the second

State of the state

Hydrogen gas is recycled from cathode to anode compartments and chloride ions pass through the (anionic) cell membrane in the same direction. Thermal regeneration occurs by distillation of the HCl out of the spent anode fluid: the HCl is returned to the cathode and the fresh MEICl goes back to the anode.

Test results demonstrated that a TRFC based on HCI/MEICI is capable of operating with a heat source at 200°C, and a cell temperature of about 100°C. In a test where hydrogen transfer from rathode to anode took place by diffusion through the cell membrane, we measured an open circuit voltage (OCV) of 206 mV and a maximum power density of 0.35 mW/cm². Although ten-times larger power densities are commonplace with aqueous TRFC cells, this is the best result we have achieved with through-membrane hydrogen transfer. When hydrogen was fed to the edge of the anode instead, the OCV was 300 mV and the maximum power density was 0.69 mW/cm².

Details of the work were published in the annual contract report for 1990. Problem areas identified during Phase I included possible decomposition of MEICI during regeneration at 200-250°C, incomplete wetting of the fuel cell anode, poor membrane conductivity and the difficulty of separating HCI gas from hydrogen. These areas became the focus of our work during Phase II.

Phase II

Differential scanning calorimetry (DSC) on a sample of MEICI showed that thermal decomposition began at about 260°C. The result was consistent with published findings that the compound is stable below 250°C². DSC could not be performed on MEIHCI₂ because the compound attacked the sample holder. Instead we analyzed the gases evolved under simulated regeneration conditions. Irreversible decomposition was confirmed at 200-250°C. The decomposition occurred by loss of alkyl groups rather than by ring opening. It could probably be suppressed by replacing the methyl and ethyl groups with larger, more stable substituents such as butyl or propyl groups.

Electrode wetting was improved by reducing the TFE content of the fuel cell anode but no adequate solutions were found to the problems of gas separation or membrane resistance.

Phase III

In view of the performance limitations associated with the HCVMEICI system, the possibilities of other working fluids were explored. In particular, Lewis acid/base systems of the type AlCl₃/MCI appeared to merit investigation. In this system, the electrode reactions are:

Chloride ions pass through the cell membrane from cathode to anode compartments. Thermal regeneration occurs by distilling AlCl₃ out of the spent anode fluid and returning it to the catholyte:

A disadvantage of the above scheme is the need to return a solid reactant (metallic aluminum) from the cathode to the anode during cell operation. The transfer would be more practical with a liquid reactant such a metallic gallium. For this reason, we chose the model system GaCl₃/MEICl to explore the feasibility of a Lewis acid/base working fluid. Funding constraints during 1991 limited the scope of the investigation to a literature review and some preliminary experiments.

We found no published information on the EMF of GaCl₃/MEICl concentration cells but such data do exist for the aluminum system³. By comparing the equilibrium constant published by Verbrugge and Carpenter (1990)⁴ for the reaction:

 $2GaCl_4$ — Ga_2Cl_7 + Cl^- K=0.3 with the equilibrium constant quoted for the corresponding AlCl₃ reaction, (K=10⁻¹⁶), we estimated that the EMF of TRFC based on GaCl₃/MEICl may reach a few hundred millivolts, with a regeneration temperature in the range 100-200°C.

Concentration cell tests were performed at room temperature in an inert atmosphere glove box. To assemble the cell, an anion-conducting membrane (Pall RAI R-1030) was clamped vertically between the two halves of a split 5-ml Teflon cup. Platinum wires passing through each side of the cup made contact with 1-ml pools of gallium in the bottom of each compartment. Mixtures of GaCl₃ and MEICl of different ratios were placed in the two compartments and the cell EMF was measured. The measured EMFs for three tests are shown in Table 1.

TABLE 1. EMF OF GaCI3 CONCENTRATION CELLS

Mole % GaCl ₃ in Anode Compartment	Mole % GaCl ₃ in Cathode Compartment	CELL EMF, VOLTS
26	86.2	2.07
40	86.1	1.75
60	86.2	0.63

Conclusions

Solventless ionic liquids show promise as possible working fluids for both low and high temperature TRFC systems. During Phase I, HCI/MEICI working fluids were found to be viable candidates for a TRFC system that can be regenerated at about 200°C. The system has the potential for becoming the most efficient and highest power density thermal to electrical energy generating device among competing low-temperature technologies. Challenges remaining to be solved include the possible decomposition of MEICI during regeneration, poor membrane conductivity and the difficulty of separating HCI gas from hydrogen.

The surprisingly large EMF values observed with GaCl₃/MEICl cells are very encouraging. They suggest that a TRFC operating on Lewis acid/base fluids may achieve energy densities several times greater than those achievable with aqueous fluids. At the same time, the regeneration temperature is likely to approach 1000°C. While this temperature is clearly too high for organic reagents, substituting NaCl for MEICl may well yield a practical high-temperature TRFC system.

References

- 1. F.A. Ludwig, C.W. Townsend, C.P. Madhusudan, "Low temperature thermoelectrochemical system and method". U.S. Patent No. 4,738,904.
- 2. John R.Stuff, "Thermal decomposition of (MEICI)/aluminum chloride molten salts", Thermochimica Acta, 152, 421-425 (1989).
- 3. C. Dymeck, Jr, J. Williams, and J. Auborn, "A concentration cell using room-temperature chloroaluminate molten salts", Extended Abstract No. 98, Electrochemical Society Proceedings 83-2, pp. 156-7 (1983).
- 4. M.W. Verbrugge and M.K. Carpenter, "Micrelectrode study of gallium deposition from chlorogallate melts", AIChE Journal, 36(7), 1097-1105 (1990).